

DSCFIT ©

*Flexible, Rapid and Automated Analysis of Differential Scanning
Calorimetry Data*

USER'S MANUAL

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Program Description

DSCFIT is designed to analyze data from differential scanning calorimetry (DSC) experiments. It uses a statistical mechanics-based two-state model in combination with an optimized non-linear least-squares fitting routine. The program is designed to be flexible, rapid, and require a minimum of operator intervention. By setting appropriate parameters, users can customize the type of model to be used in fitting the data. **DSCFIT** has the unique ability to evaluate concentration errors in DSC data, in addition to the determination of *van't Hoff* and calorimetric enthalpies.

System Requirements and Limitations

DSCFIT is a Windows™ 95/98/NT based program. A graphics display of at least 800x600 is required. A minimum of 32 MB of system memory is also required. The disk space requirements of the program are quite modest (currently <5 MB). As currently implemented, **DSCFIT** can analyze data sets with 2000, or fewer, data points. Data from both upscan and downscan experiments can be analyzed.

Please report all bugs, etc. to:

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Suggestions for improvements to **DSCFIT** are also welcome.

How to Use this Manual

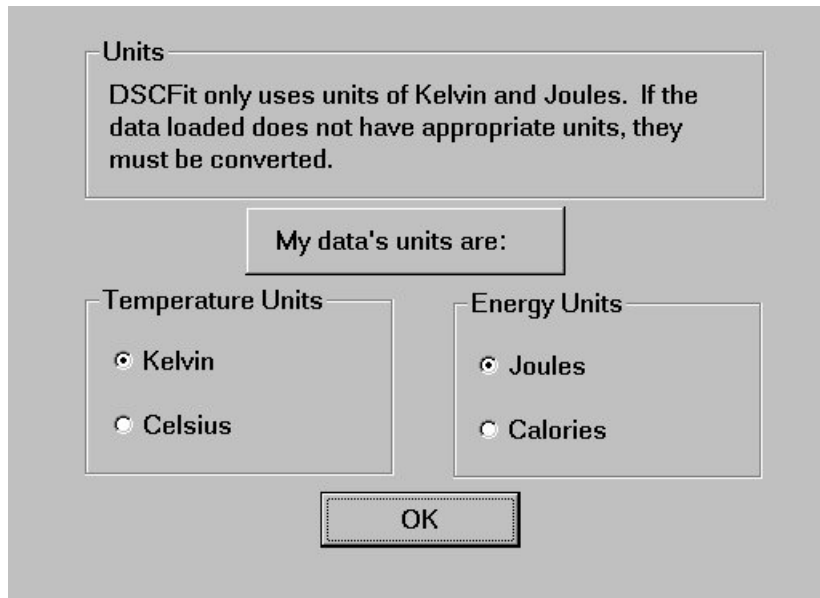
If you are ready to analyze a data set, proceed to section 1 (General Steps in Data Analysis). General descriptions of thermodynamic parameters are found in Section 2, and derivations of the thermodynamics parameters are found in Section 5. Section 3 (Available Models) and Section 4 (Advanced Topics) provide information on the various features of the program and their application in data analysis.

Section 1: General Steps in Data Analysis

I. Loading of Data

The DSC data to be analyzed in *DSCFIT* should be a finalized molar heat capacity data file. In other words, it should be a protein/buffer run that has had the buffer/buffer run subtracted, and then been normalized for the molar concentration of the protein (although, as discussed in the **Advanced Concepts** section, *DSCFIT* can determine the apparent molar concentration with certain assumptions). The data file should be a text file consisting of two columns: the first column will contain the temperature data, and the second column will contain the corresponding values for the molar heat capacity. These columns of data may be separated by either a space (or spaces) or a tab character. *DSCFIT* will not currently parse data delineated by other characters (e.g. commas). The temperature can be either in °C or K, and the molar heat capacity can be in either calorie or Joule units (*DSCFIT* works internally with K and Joules, however).

Load data by using either the File→Load Data menu command, or the "Load Data" command on the menu bar. A dialog window will open enabling you to specify the desired data file (the default file extension is *.dat). When reading in the data file, *DSCFIT* will present you with a dialog box to allow conversion of °C or calorie-based data to K and Joules:



Select the appropriate radio buttons for the units of the input data (in cases where the temperature appears to be in °C rather than K, *DSCFIT* will alert the user to the need to convert). The temperature and heat capacity units are independent. Thus, if for some bizarre reason your raw data is in °C and Joules, select the radio buttons for Celsius and Joules.

After reading the data file, **DSCFIT** will report the number of successfully imported data points, and the temperature range of the data:

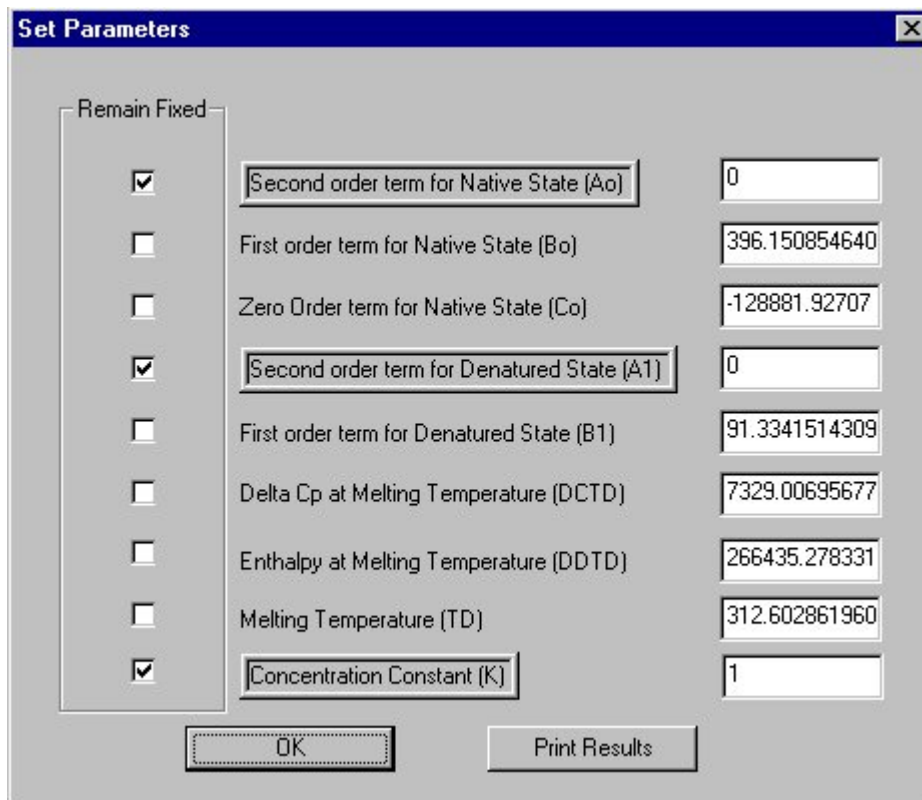


Before continuing, be sure that this information is as expected for the data file in question.

Note: Currently, **DSCFIT** applies the conversions of $K=(273.15+^{\circ}C)$, and $Joules=(calories/4.184)$ directly to the data when imported. If a mistake is made with the units when importing the data, close the project window and read in the data file again.

II. Initial Guess of Thermodynamic Parameters

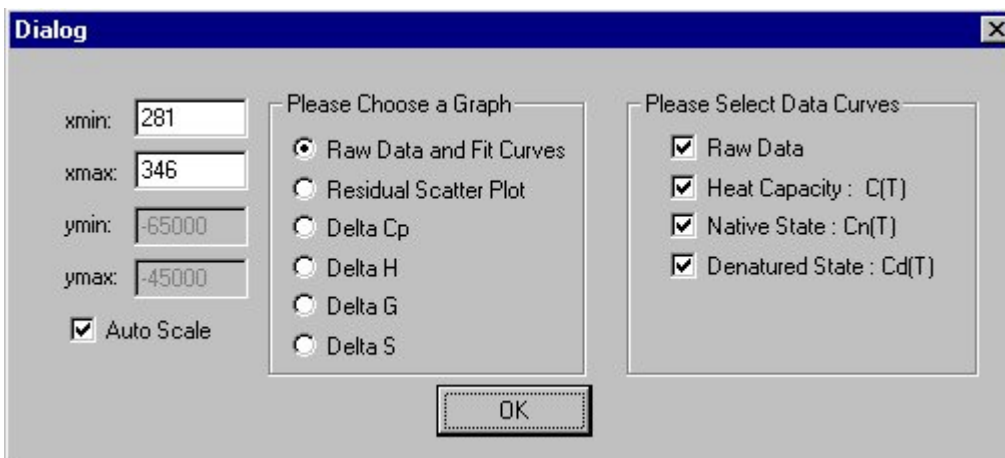
After reading in a data file **DSCFIT** will automatically determine an initial guess for the various thermodynamic parameters, and report these values in the **Parameters Dialog Box**:



At this point you can simply click 'OK' to accept the program's initial guesses for the parameters. Alternatively, you can modify any of the parameters. Checking the left-hand side box next to a parameter will constrain the parameter during refinement to the value indicated in the right-hand side box. Leaving the left-hand side box unchecked will allow the value of the parameter to vary during refinement to improve the agreement of the model with the data. Three parameters, A_0 (the second order term for the native state heat capacity function), A_1 (the second order term for the denatured state heat capacity), and k (the concentration constant) are constrained (as indicated by the appropriately checked box) to values of 0, 0, and 1, respectively. The text descriptions of these parameters are also boxed, to indicate that **refinement of these parameters may be justified only under certain circumstances**.

III. Graphs Dialog Box

After assignment of the initial values for the various thermodynamic parameters **DSCFIT** will display the **Graphs Dialog Box**:



The Graphs Dialog Box allows you to select the appropriate thermodynamic function(s) for viewing as a graph. The graph chosen will be actively updated during the refinement cycle. The available functions include:

Raw Data and Fit Curves - this graph will include the raw data and can also include the functions for the native state heat capacity function, denatured state heat capacity function as well as the fitted function based upon the current values of the various thermodynamic variables. This is the default graphic representation.

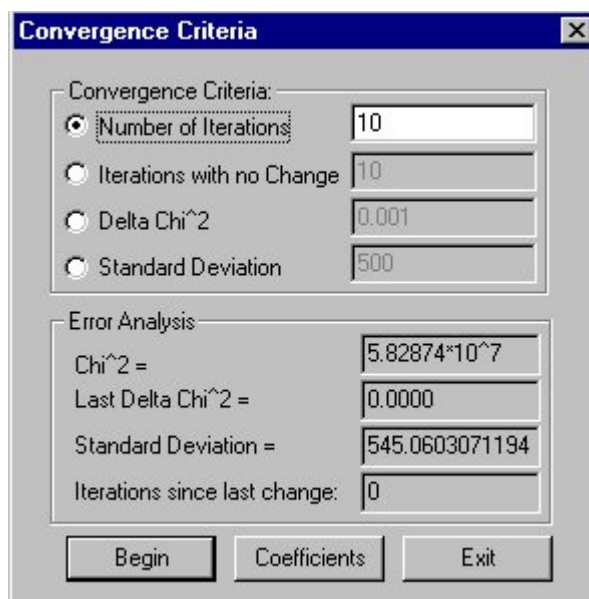
Residual Scatter Plot - this graph shows the disagreement between the fitted function and the raw data. It is useful for determining the magnitude of the error (i.e. whether it is within the expected instrumentation noise level) and whether the error is random, or systematic (indicating possible non-2-state behavior).

Delta C_p, Delta H, Delta G, Delta S - plots for these thermodynamic functions.

On the left-hand side of the Graphs Dialog Box are parameters used in graphic the various functions. The default values are to autoscale Y, and the temperature range is the minimum and maximum of the data points.

V. Refine Dialog Box

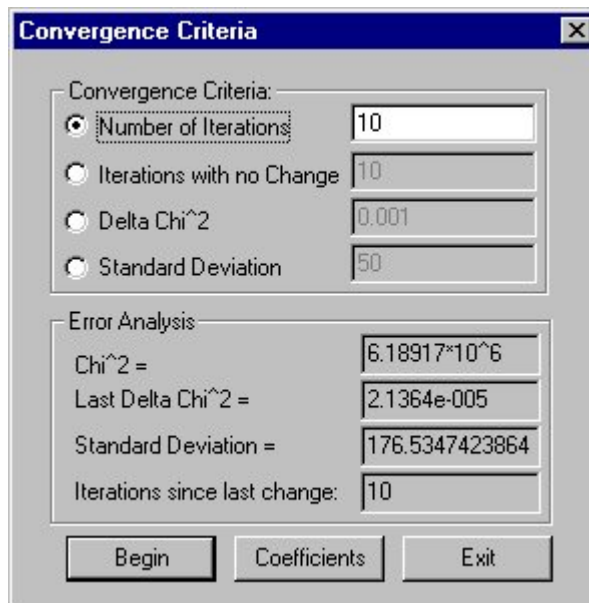
After the appropriate graph has been selected the graph will be shown, along with the **Refine Dialog Box**:



The Refine Dialog Box allows you to select the criteria for convergence of the model fit to the experimental data. The choices include: 1) refine for a fixed number of cycles, or 2) refine until no further improvement in the merit function is observed over a given number of refinement cycles, or 3) refine until the improvement in the merit function decreases to a specified value, or 4) refine until the standard deviation of the fit decreases to a specified value. Additionally, there is a button labeled **Coefficients**. Selecting this button will bring up the Coefficients Dialog Box (where the values of the various thermodynamic parameters can be manually entered, or the **constrain** check boxes may be selected or deselected).

Clicking the button labeled **'Begin'** will start the refinement of the thermodynamic parameters (to improve the fit with the raw data). The refinement will proceed until the selected criteria for convergence has been met. If more than 100 cycles of refinement are performed without the convergence criteria being met, the program will exit from refinement with an alert message.

Statistical information on the refinement is available within **Error Analysis** section of the **Refine Dialog Box**:



The information includes: 1) the value of the χ^2 merit function, 2) the last value observed for the change in the merit function, 3) the standard deviation of the fit to the experimental data, and 4) the number of iterations that have occurred since an improvement in the merit function was observed.

Each time the refinement routine identifies values that improve the agreement of the model with the raw data the currently displayed graph will be updated. When is the refinement of the thermodynamic parameters complete? As refinement proceeds, the value for the χ^2 merit function should decrease, although a target value is difficult to know in advance. The value for $\Delta\chi^2$ should also decrease, with values typically smaller than 1×10^{-5} typical of convergence. The standard deviation should also decrease. Target values for the standard deviation would be related to the expected error for the instrument (e.g. on the order of 100-200 J mol⁻¹ K⁻¹). If the fit has converged, many cycles (i.e. >10) of refinement will occur without an improvement in the fit.

Clicking on the **Coefficients** button in the **Refine Dialog Box** will bring up the Coefficients Dialog Box from which the values for the refined thermodynamic parameters can be read:

Parameter	Value
Second order term for Native State (Ao)	0
First order term for Native State (Bo)	435.449870637
Zero Order term for Native State (Co)	-128027.72383
Second order term for Denatured State (A1)	0
First order term for Denatured State (B1)	99.9690809707
Delta Cp at Melting Temperature (DCTD)	6497.17706293
Enthalpy at Melting Temperature (DDTD)	257266.416858
Melting Temperature (TD)	312.566703903
Concentration Constant (K)	1

Section 2: Description of Thermodynamic Parameters

I. A_0 , B_0 , C_0

The native state heat capacity function, $C_N(T)$, is defined by the following function:

$$C_N(T) = 3 \cdot A_0 \cdot (T - TD)^2 + 2 \cdot B_0 \cdot (T - TD) + C_0$$

where TD is the melting temperature. Thus, $C_N(T)$ is a second-order polynomial when A_0 is non-zero. **If A_0 is constrained to a value of 0** (default value for A_0), **$C_N(T)$ is a linear function.** Likewise, **if both A_0 and B_0 are constrained to values of 0, $C_N(T)$ is a constant.** In any case, **C_0 is the value of $C_N(T)$ at the TD.**

II. A_1 , B_1 , DCTD

The denatured state heat capacity function, $C_D(T)$, is defined by the following function:

$$C_D(T) = 3 \cdot A_1 \cdot (T - TD)^2 + 2 \cdot B_1 \cdot (T - TD) + (DCTD + C_0)$$

where TD is the melting temperature. Thus, $C_D(T)$ is a second-order polynomial when A_1 is non-zero. **If A_1 is constrained to a value of 0** (default value for A_1), **$C_D(T)$ is a linear function**. Likewise, **if both A_1 and B_1 are constrained to values of 0, $C_D(T)$ is a constant**. **DCTD** is the value of $\Delta C_p(T)$ at the TD. Since $\Delta C_p(T)$ is defined at $C_D(T) - C_N(T)$, and C_0 is the value of $C_N(T)$ at the TD, **(DCTD + C_0) is equal to the value of $C_D(T)$ at the TD**.

III. DDTD

DDTD is defined by the following function:

$$\Delta H(T) = (A_1 - A_0) * (T - TD)^3 + (B_1 - B_0) * (T - TD)^2 + DCTD * (T - TD) + DDTD$$

Thus, **DDTD is the value of $\Delta H(T)$ at the TD**.

IV. TD

Formally, it is the temperature at which the native and denatured states are equally populated. TD must exist. In other words, the model requires that there be some definite temperature at which the native and denatured states are equally populated. If the conditions are such that the native is never more than 50% populated, the analysis will fail.

V. k

The k parameter is a scalar term applied to the raw data molar heat capacity. If it is allowed to float during refinement, and does not refine to a value of 1.0, there are two possible interpretations:

1. $\Delta H_{vH} / \Delta H_{cal} = 1.0$, but the concentration applied during normalization of the molar heat capacity is incorrect. In this case, **the actual concentration of the protein in the DSC analysis is: (the value used during the normalization / k)**. Furthermore, the refined thermodynamic parameters are for the **corrected** concentration.
2. The concentration is correct, but ΔH_{vH} is not equal to ΔH_{cal} . In this case, the value of **k is equal to $(\Delta H_{vH} / \Delta H_{cal})$** . Furthermore, **the refined value of DDTD is equal to ΔH_{vH}** . **ΔH_{cal} can be derived by dividing DDTD (van't Hoff enthalpy) by k** .

Thus, **k should only be allowed to float if other data is available to confirm either the concentration, or the value of $\Delta H_{vH} / \Delta H_{cal}$** (see Advanced Topics section).

Section 3: Available Models

DSCFIT is customizable to allow a variety of treatments for the $C_N(T)$ and $C_D(T)$ functions, as well as the $\Delta C_p(T)$ and $\Delta H(T)$ functions).

I. $C_N(T)$

$C_N(T)$ can be modeled as either a second-order polynomial, linear function or constant (independent of the treatment of the $C_D(T)$ function):

A_0 is non-zero: $C_N(T)$ is a second-order polynomial

$A_0 = 0$: $C_N(T)$ is a linear function (slope = B_0 , y intercept = C_0)

A_0 and $B_0 = 0$: $C_N(T)$ is a constant equal to C_0

Values for A_0 , B_0 and C_0 can be allowed to float during refinement, or may be fixed at some operator defined value (the model will find the best function with these applied constraints).

II. $C_D(T)$

Like $C_N(T)$, $C_D(T)$ can be modeled as either a second-order polynomial, linear function or constant (independent of the treatment of the $C_N(T)$ function):

A_1 is non-zero: $C_D(T)$ is a second-order polynomial

$A_1 = 0$: $C_D(T)$ is a linear function (slope = B_1 , y intercept = C_1)

A_1 and $B_1 = 0$: $C_D(T)$ is a constant equal to $(DCTD + C_0)$

Values for A_1 and B_1 can be allowed to float during refinement, or may be fixed at some operator defined value (the model will find the best function with these applied constraints).

III. DCTD

DCTD defines the value of $\Delta C_p(T)$ at the TD. This value can be fixed or allowed to float during refinement. Of all the thermodynamic parameters, this is the most difficult value to determine accurately, and is sensitive to errors in concentration determination. In some cases, i.e. where accurate values for $\Delta C_p(T)$ at the TD are known, it may be appropriate to refine with the value for DCTD constrained to the known value.

The nature of the $\Delta C_p(T)$ function is defined by the $C_N(T)$ and $C_D(T)$ functions (i.e. $\Delta C_p(T) = C_D(T) - C_N(T)$). Thus, if both $C_N(T)$ and $C_D(T)$ functions are linear, then $\Delta C_p(T)$ will be a linear function, etc.

IV. DDTD and TD

If desired, the value of $\Delta H(T)$ at the TD can be constrained. Also, the value of TD can be constrained.

V. k

As discussed in the **Description of Thermodynamic Parameters** the k parameter is a scalar term applied to the raw data molar heat capacity. Investigators can use the refined value of k to gauge potential errors in concentration and inequality of ΔH_{vH} and ΔH_{cal} . If it is allowed to float during refinement, and does not refine to a value of 1.0, there are two possible interpretations:

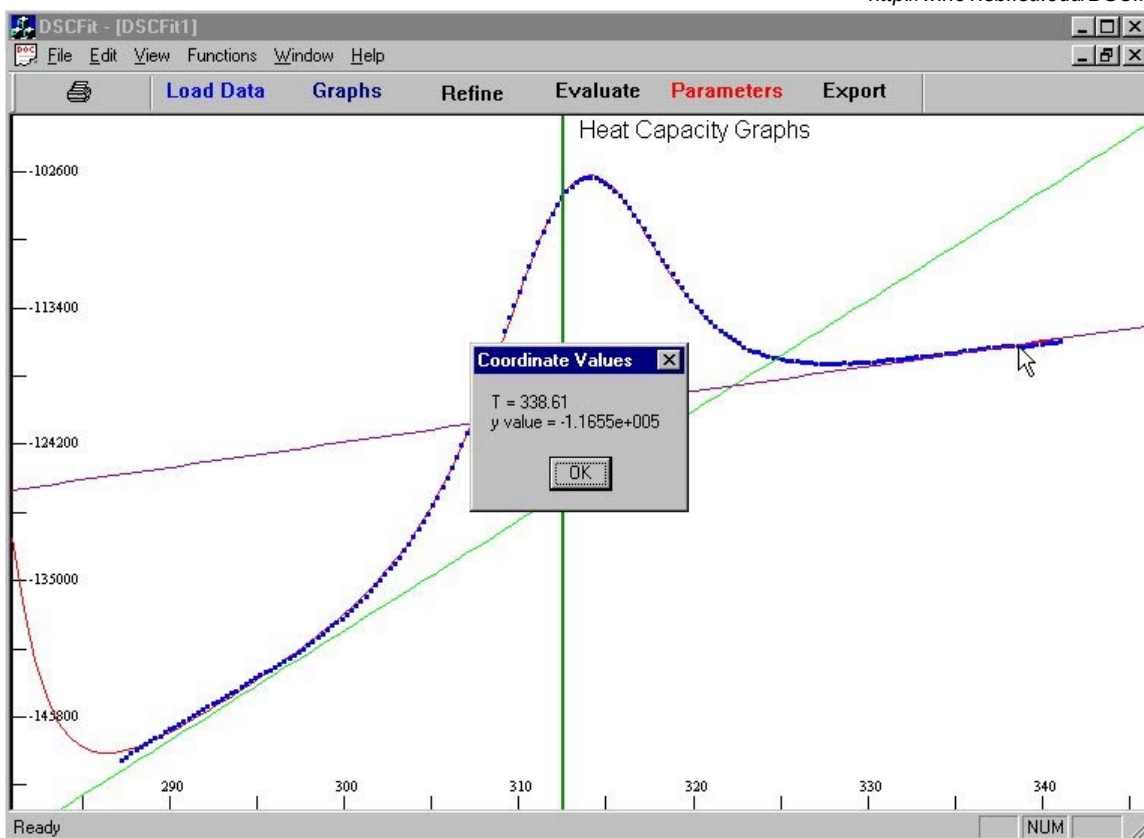
1. $\Delta H_{vH}/\Delta H_{cal} = 1.0$, but the concentration applied during normalization of the molar heat capacity is incorrect. In this case, **the actual concentration of the protein in the DSC analysis is: (the value used during the normalization / k)**. Furthermore, the refined thermodynamic parameters are for the **corrected** concentration.
2. The concentration is correct, but ΔH_{vH} is not equal to ΔH_{cal} . In this case, the value of **K is equal to $(\Delta H_{vH}/\Delta H_{cal})$** . Furthermore, **the refined value of DDTD is equal to ΔH_{vH}** . ΔH_{cal} can be derived by dividing DDTD (van't Hoff enthalpy) by k .

Thus, ***k should only be allowed to float if other data is available to confirm either the concentration, or the value of $\Delta H_{vH}/\Delta H_{cal}$*** (see Advanced Topics section).

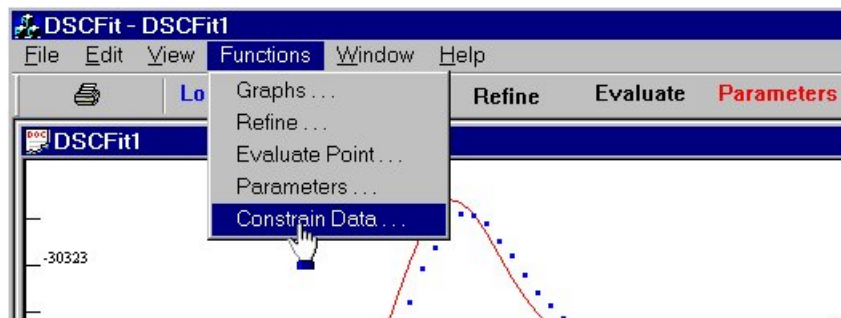
Section 4: Advanced Topics

I. Data Clipping

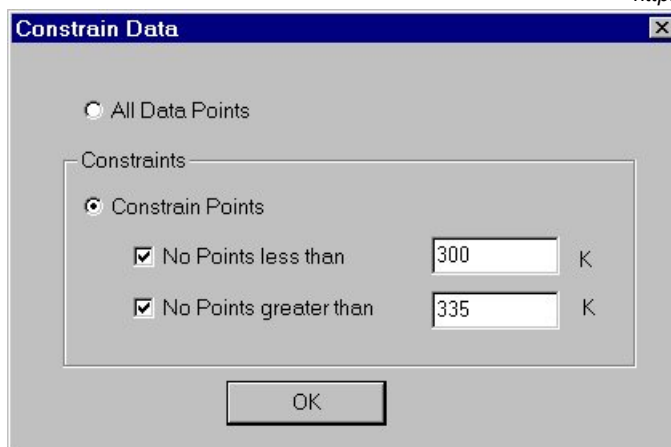
The range of data to be analyzed can be defined using both a high and low temperature cutoff value. The first step is to identify the temperature range(s) for exclusion. Place the mouse pointer at the appropriate position in any of the displayed graphs and **click the right mouse button** to obtain the x,y coordinates of that point:



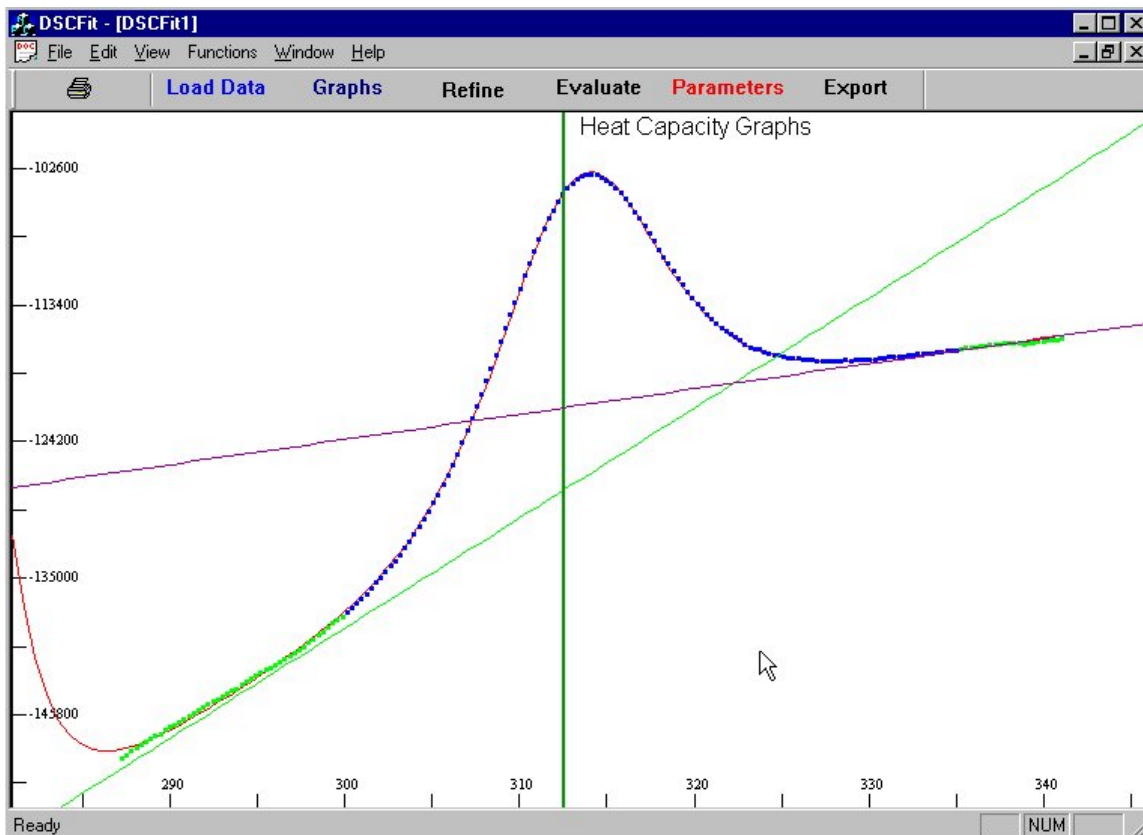
Once the specific high and low temperature cutoff values have been identified, you can limit the data range used during refinement by selecting the **Functions**→**Constrain Data...** options from the menu bar:



This will bring up the **Constrain Data Dialog** box:



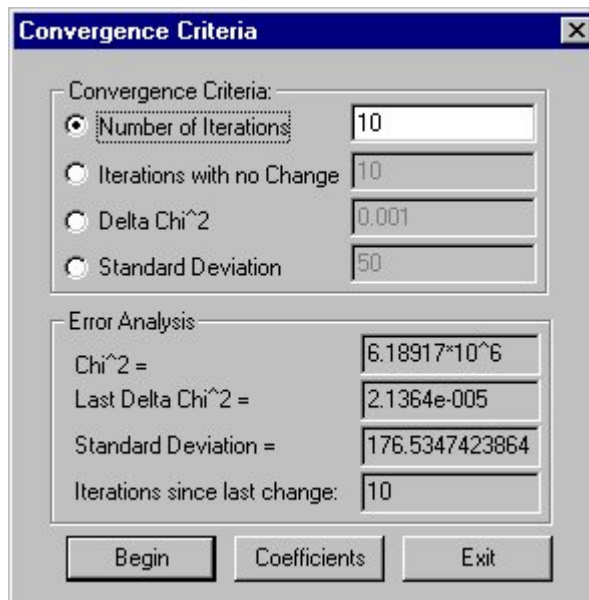
Select the **Constrain Points** radio button to constrain the region of data for analysis, then enter the low and high temperature cutoff values (in K). When the data is subsequently graphed, the cutoff data regions will be displayed in green and the active data points remain blue:



II. Evaluation of Non-2-state Behavior

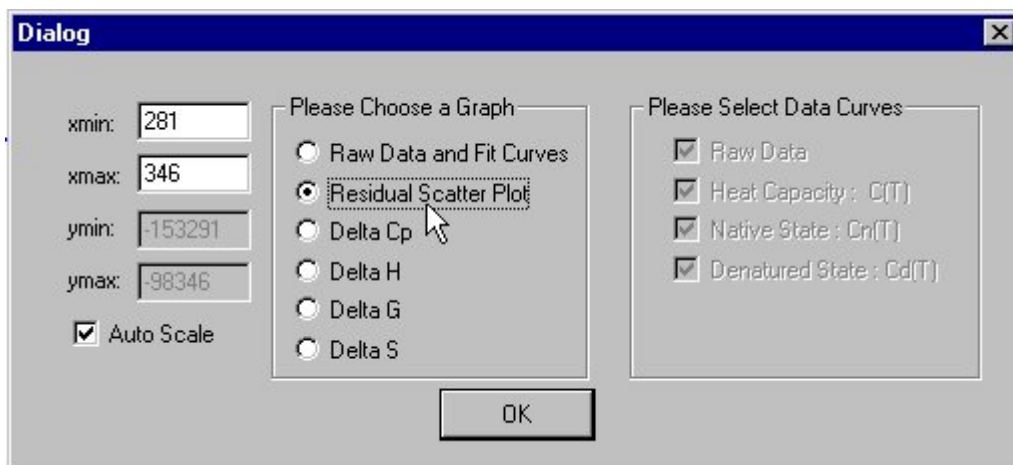
Various criteria are used to determine whether the experimental data agrees with the 2-state assumption of the model. The first relates to the deviation of the raw data from the refined model. This deviation is evaluated by

noting the value of the **Standard Deviation** in the **Refine Dialog Box** and comparing this value to the expected instrumentation noise:

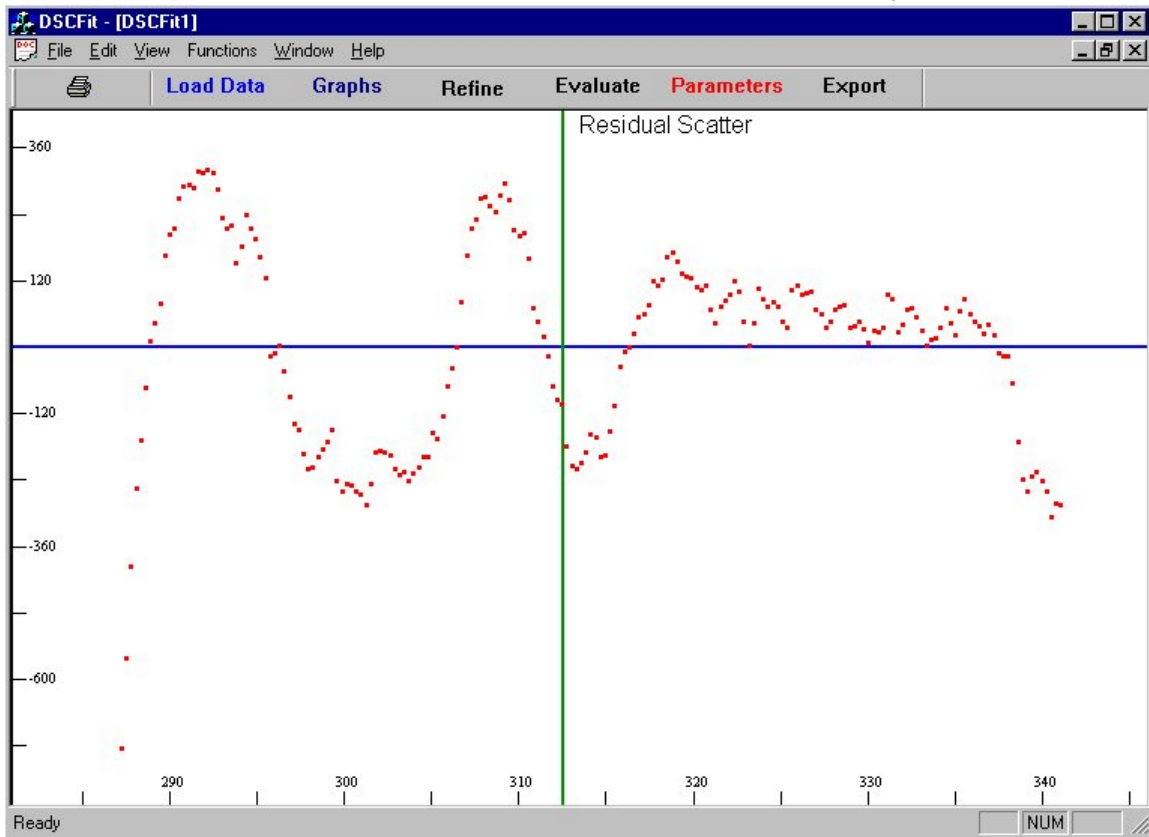


Standard Deviation values around $100 \text{ J mol}^{-1} \text{ K}^{-1}$ represent an excellent fit with 2-state behavior. Typical values range around $100\text{-}500 \text{ J mol}^{-1} \text{ K}^{-1}$. Values above $500 \text{ J mol}^{-1} \text{ K}^{-1}$ may indicate non-2-state behavior.

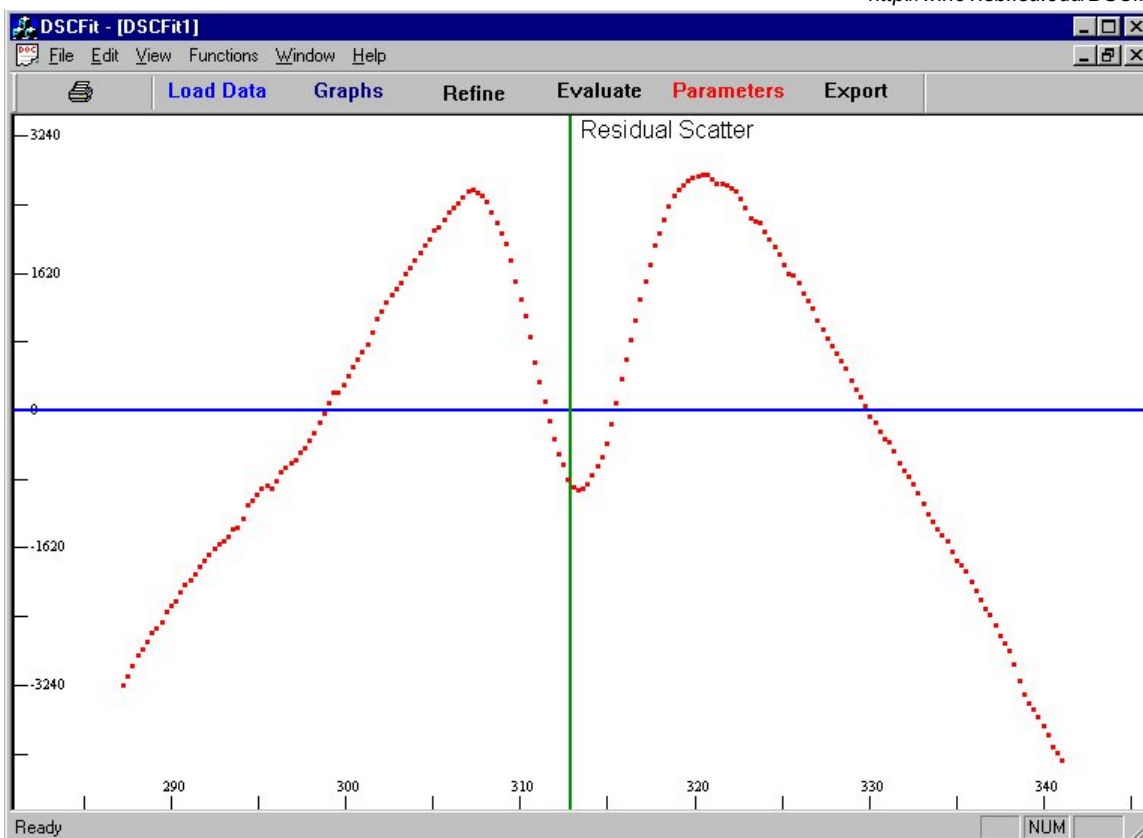
Another property to evaluate is the **residual scatter** of the data, and to decide whether it is random or systematic. The residual scatter of the data is a graphical representation of the difference between the fitted model and the raw data (fit - raw data). Select the **Residual Scatter Plot** radio button from the **Graphs** dialog box (selected from the Graphs menu button):



A graph of the residual scatter will be displayed. This graph will include a vertical green line to indicate the location of the melting temperature (TD), as well as a blue horizontal line indicating the zero location of the scatter:



Non-random distribution of the scatter can be indicative of non-2-state behavior. A peak, or trough, centered at the TD is one of the features of a transition that is too broad, or too narrow, to be fit by a 2-state model:



In this example the transition of the raw data is too broad for a 2-state model. Thus, the fit tends to overshoot the peak of the raw data, and undershoot on either side of the peak. In addition to the systematic nature of the residual scatter, the magnitude of the error is greater (compare to prior scatter plot).

Non-2-state behavior, due to an intermediate state, can also result in aberrant values for $\Delta C_p(T)$ at the TD. In particular, apparent **negative** values for ΔC_p at the TD (i.e. the value of the **DCTD** parameter) may result:

Parameter	Value
Second order term for Native State (Ao)	0
First order term for Native State (Bo)	503.753807744
Zero Order term for Native State (Co)	-123418.92982
Second order term for Denatured State (A1)	0
First order term for Denatured State (B1)	174.891326096
Delta Cp at Melting Temperature (DCTD)	-1006.5455466
Enthalpy at Melting Temperature (DDTD)	262950.118815
Melting Temperature (TD)	314.070507679
Concentration Constant (K)	1

In this case, residual structure leads to residual enthalpy after the main transition. This causes an aberrantly large positive slope for the $C_D(T)$ function. Thus, at the TD the $C_D(T)$ function may actually appear to be lower than the $C_N(T)$ function (resulting in a negative value for ΔC_p).

Finally, the k parameter can be refined (instead of being constrained to 1) to evaluate the possibility of non-2-state behavior. In this case, ***it is essential that the concentration of the sample be accurate!*** If k is allowed to float during refinement, and does not refine to a value of 1.0, there are two possible interpretations:

1. $\Delta H_{vH}/\Delta H_{cal} = 1.0$, but the concentration applied during normalization of the molar heat capacity is incorrect. In this case, **the actual concentration of the protein in the DSC analysis is: (the value used during the normalization / k)**. Furthermore, the refined thermodynamic parameters are for the **corrected** concentration.
2. The concentration is correct, but ΔH_{vH} is not equal to ΔH_{cal} . In this case, the value of k is equal to $(\Delta H_{vH}/\Delta H_{cal})$. Furthermore, **the refined value of DDTD is equal to ΔH_{vH} . ΔH_{cal} can be derived by dividing DDTD (van't Hoff enthalpy) by k .**

Parameter refinement of the prior data set, with k allowed to float, results in a value for k of 0.80, indicating a $\Delta H_{vH}/\Delta H_{cal}$ ratio consistent with non-2-state behavior (i.e. the presence of an intermediate state).

Thus, the evaluation of non-2-state behavior relies upon analysis of:

- The magnitude of the standard deviation
- The nature of the residual scatter (random vs. systematic)
- The value of ΔC_p at the TD
- The value of the refined K parameter (i.e. $\Delta H_{VH}/\Delta H_{cal}$)

III. Use of Second-order Polynomial Functions for $C_N(T)$ or $C_D(T)$

DSCFIT allows the option of the use of second-order polynomial functions for the $C_N(T)$ and $C_D(T)$ functions. The general paradigm of protein denaturation, for example, is that the $C_N(T)$ function is well approximated by a linear function, while the $C_D(T)$ function may exhibit slight curvature. However, over the typical temperature ranges used to study protein thermal denaturation, this curvature is slight and a linear function is a reasonable approximation for the $C_D(T)$ function. The following is an example of the application of a second-order polynomial for the $C_D(T)$ function for a data set of human acidic fibroblast growth factor. First, the refinement is performed with a linear function for both $C_N(T)$ and $C_D(T)$:

Parameter	Value
<input checked="" type="checkbox"/> Second order term for Native State (Ao)	0
<input type="checkbox"/> First order term for Native State (Bo)	435.449870341
<input type="checkbox"/> Zero Order term for Native State (Co)	-128027.72382
<input checked="" type="checkbox"/> Second order term for Denatured State (A1)	0
<input type="checkbox"/> First order term for Denatured State (B1)	99.9690814087
<input type="checkbox"/> Delta Cp at Melting Temperature (DCTD)	6497.17704232
<input type="checkbox"/> Enthalpy at Melting Temperature (DDTD)	257266.416971
<input type="checkbox"/> Melting Temperature (TD)	312.566703908
<input checked="" type="checkbox"/> Concentration Constant (K)	1

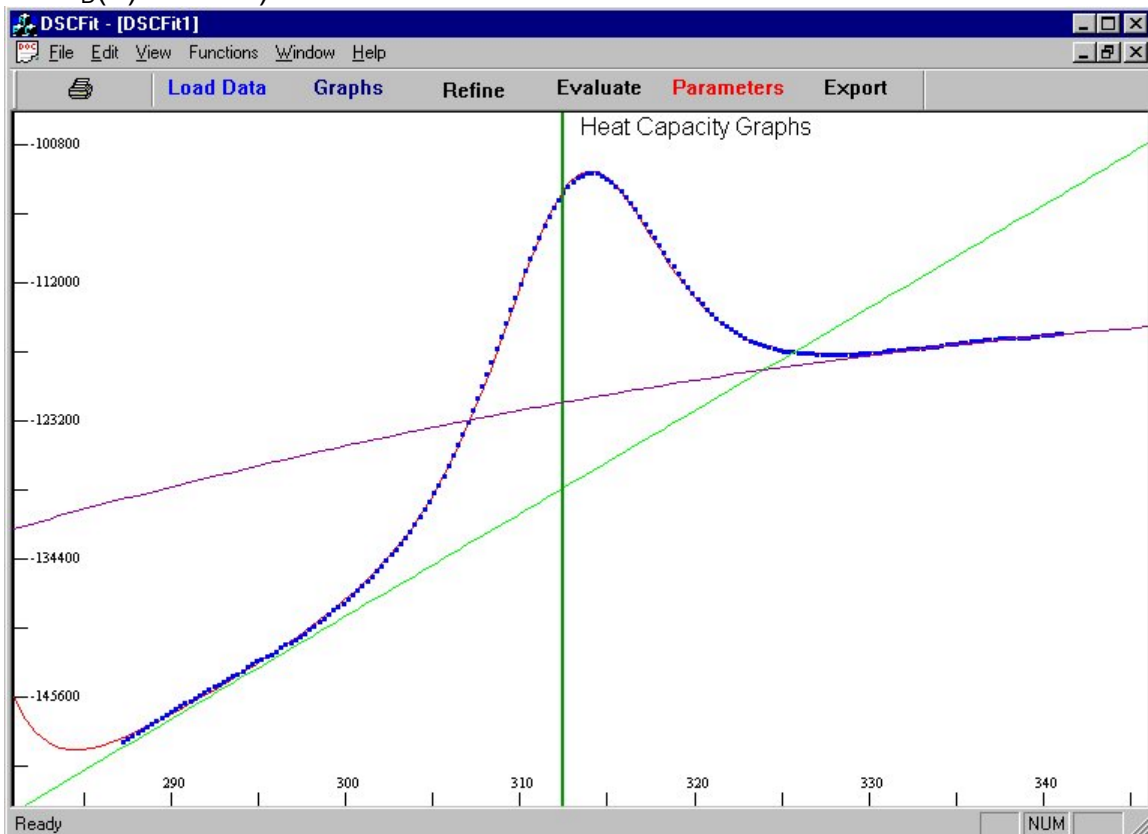
Now A_1 is allowed to float during refinement, thus $C_D(T)$ will be a second-order polynomial:

Set Parameters

Remain Fixed	Parameter	Value
<input checked="" type="checkbox"/>	Second order term for Native State (Ao)	0
<input type="checkbox"/>	First order term for Native State (Bo)	417.286919434
<input type="checkbox"/>	Zero Order term for Native State (Co)	-128673.63922
<input type="checkbox"/>	Second order term for Denatured State (A1)	-0.7301307263
<input type="checkbox"/>	First order term for Denatured State (B1)	128.174880682
<input type="checkbox"/>	Delta Cp at Melting Temperature (DCTD)	6976.44295027
<input type="checkbox"/>	Enthalpy at Melting Temperature (DDTD)	258322.627223
<input type="checkbox"/>	Melting Temperature (TD)	312.435822846
<input checked="" type="checkbox"/>	Concentration Constant (K)	1

OK Print Results

The fitted function and $C_N(T)$ and $C_D(T)$ functions look like this (note the curve of the $C_D(T)$ function):



Although **DSCFIT** allows the use of second-order polynomials during the refinement, **it is up to the user to decide if the use of a second-order polynomial is valid**. The key issue is the **accuracy of the baselines at temperatures far away from the TD**. The use of second-order polynomial baselines can result in unreasonable behavior at extremes of temperature. Thus, **while second-order polynomial functions for $C_D(T)$, or $C_N(T)$, may improve accuracy at the TD, the accuracy at other temperatures may be reduced**.

IV. Determination of Thermodynamic Constants at Temperatures other than TD

It is often important to evaluate the values for the various thermodynamic constants at temperatures other than the TD. For example, determination of the effects of a destabilizing, or stabilizing, mutation requires that the ΔG value for the mutant be determined at the TD of the wild-type protein (to obtain a $\Delta\Delta G$ value). The value of the various thermodynamic parameters, at any reference temperature, can be obtained by using the **Functions**→**Evaluate Point...** menu or the **Evaluate** menu button. This will bring up the **Evaluate dialog box**:

Parameter	Value
Temperature	300
Raw Data	-1.38019*10 ⁵
Heat Capacity	-1.37662*10 ⁵
Delta Cp	1.38283*10 ⁴
Delta H	1.28257*10 ⁵
Delta G	7.94099*10 ³

Input the desired reference temperature (in K) in the **Temperature** box, and click the **Submit** button. The values for the various thermodynamic parameters at this reference temperature will be displayed.

V. More than One Possible Solution for Refined Parameters

Two cases have been observed where alternative solutions have been obtained during refinement. Both cases can occur when the initial guess values are poor. This situation will typically not occur if the default initial guess values are used, but may occur with operator selected values. The first case is a mathematically equivalent solution, but where the sign of DDTD and DCTD parameters are inverted. This can be demonstrated using the data set from the

discussion of the previous section, inverting the sign of DDTD and DCTD, and refining:

Parameter	Value
Second order term for Native State (Ao)	0
First order term for Native State (Bo)	99.9690830451
Zero Order term for Native State (Co)	-121530.54685
Second order term for Denatured State (A1)	0
First order term for Denatured State (B1)	435.449869195
Delta Cp at Melting Temperature (DCTD)	-6497.1769654
Enthalpy at Melting Temperature (DDTD)	-257266.41741
Melting Temperature (TD)	312.566703927
Concentration Constant (K)	1

Note that an equivalent solution has been found for the magnitude of DDTD and DCTD parameters, but that the signs are inverted. The fitted function will be equivalent to the "correct" solution.

The second situation involves an apparent local minimum for the refined parameters when the initial guesses are poor, and second order polynomials for $C_N(T)$ and $C_D(T)$ are used. This has been observed only rarely. To avoid this potential problem, **always refine using linear baselines first, then refine with second-order polynomial functions** if desired. **To confirm that the solution is not a local minimum when using second-order polynomial functions, perform several rounds of refinement, switching back and forth between linear and second-order functions for $C_N(T)$ and $C_D(T)$.**

VI. Situations Where TD Does Not Exist

Various definitions in the model depend upon a temperature value for TD. Data can be analyzed under conditions where the protein is significantly destabilized. However, **the data cannot be accurately analyzed if there is no temperature at which the native and denatured states are equally populated** (i.e. no TD).

Section 5: Derivations

Native state and denatured state heat capacity functions:

$$C_N(T) = 3 * A_0 (T - TD)^2 + 2 * B_0 (T - TD) + C_0$$

$$C_D(T) = 3 * A_1 (T - TD)^2 + 2 * B_1 (T - TD) + (DCTD + C_0)$$

$\Delta C_p(T)$ is:

$$\Delta C_p(T) = 3 * (A_1 - A_0) * (T - TD)^2 + 2 * (B_1 - B_0) * (T - TD) + DCTD$$

Thus, $\Delta H(T)$ can be written as:

$$\Delta H(T) = (A_1 - A_0) * (T - TD)^3 + (B_1 - B_0) * (T - TD)^2 + DCTD * (T - TD) + DDTD$$

$\Delta S(T)$ is:

$$\Delta S(T) = \left[\left(\ln(T) - \ln(TD) + \frac{3}{2} \right) * TD^2 - 2 * T * TD + \frac{1}{2} T^2 \right] * 3 * (A_1 - A_0) +$$

$$\left[(-1 + \ln(TD) - \ln(T)) * TD + T \right] * 2 * (B_1 - B_0) + (\ln(T) - \ln(TD)) * DCTD + \frac{DDTD}{TD}$$

and ΔG :

$$\Delta G = \Delta H - (T * \Delta S)$$

This treatment now allows us to describe the model function using the following parameters:

$$A_0, B_0, C_0, A_1, B_1, DCTD, DDTD, TD$$

Where A_0, B_0, C_0 are terms for the second order polynomial describing the native state heat capacity function, A_1, B_1 , are the first two terms for the second order polynomial describing the denatured state heat capacity function, $DCTD$ is the value of ΔC_p at the melting temperature, $DDTD$ is the enthalpy of the system at the melting temperature, and TD is the melting temperature.

This allows us to independently define the native and denatured state baselines as being either second order polynomial functions, linear functions or some constant value. It also allows us to set ΔC_p at the melting temperature (i.e. $DCTD$) and ΔH at the melting temperature (i.e. $DDTD$) to some fixed value during parameter refinement. Thus, we now have a very flexible model, with complete control over all critical parameters during refinement.

The fractional component of native state as a function of ΔG is equal to:

$$F_N(T) = \left[1 + \exp\left(-\frac{\Delta G}{RT}\right) \right]^{-1}$$

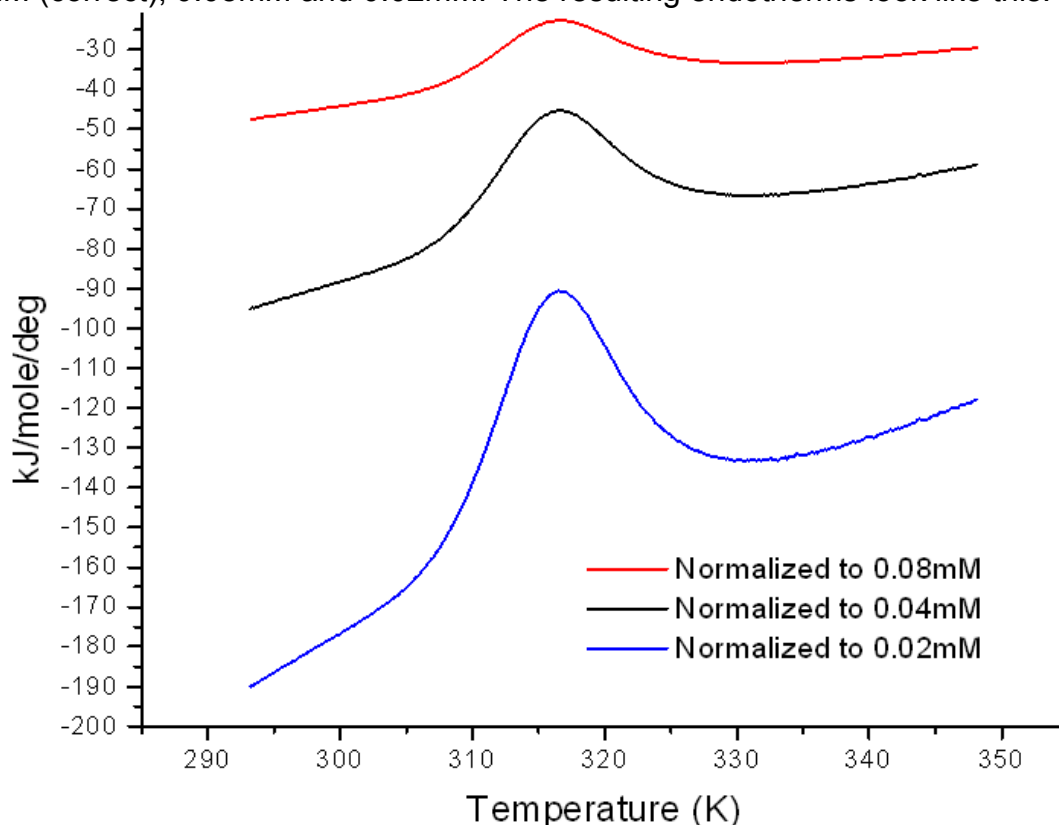
By knowing the native state heat capacity function ($C_N(T)$), the difference heat capacity function between the denatured and native states (ΔC_p), the fractional component of native state as a function of temperature, and the enthalpy function, the heat capacity of the system as a function of temperature can be determined:

$$C(T) = C_N(T) + \Delta C_p * (1 - F_N) + \left(\frac{H_{sys}(T)^2 * F_N * (1 - F_N)}{RT^2} \right)$$

Note: this equation should model your raw heat capacity data

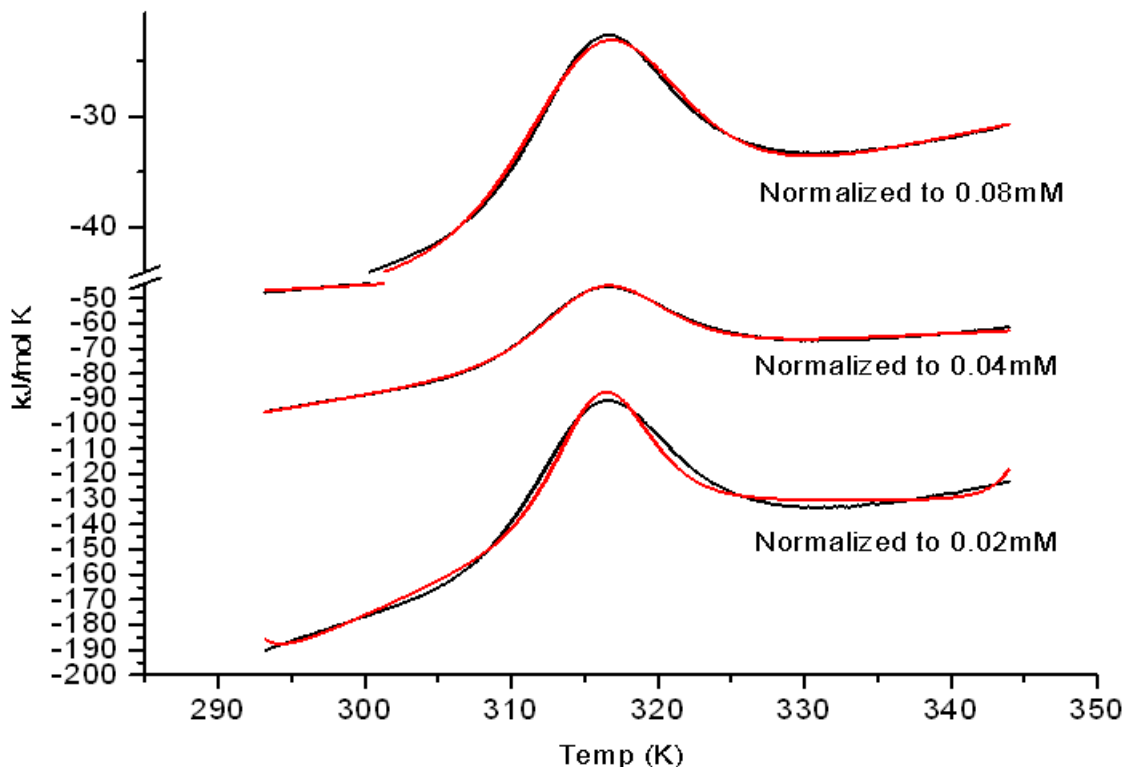
A Modification to Allow for the Determination of the van't Hoff to Calorimetric Enthalpy, or to Determine the Error in Concentration of the Protein Sample

What happens if an inaccurate value for the protein concentration is used during the normalization of DSC data? How does this affect the fitted thermodynamic parameters, and how can this be evaluated in the analysis? In the following example, the protein in the DSC experiment is determined to be 0.04mM. However, during analysis of the data, the heat capacity is normalized to three different concentrations: 0.04mM (correct), 0.08mM and 0.02mM. The resulting endotherms look like this:



Fitting our model to this data we get the following results:

0.04mM Protein Sample: Normalized to either 0.02, 0.04 or 0.08mM



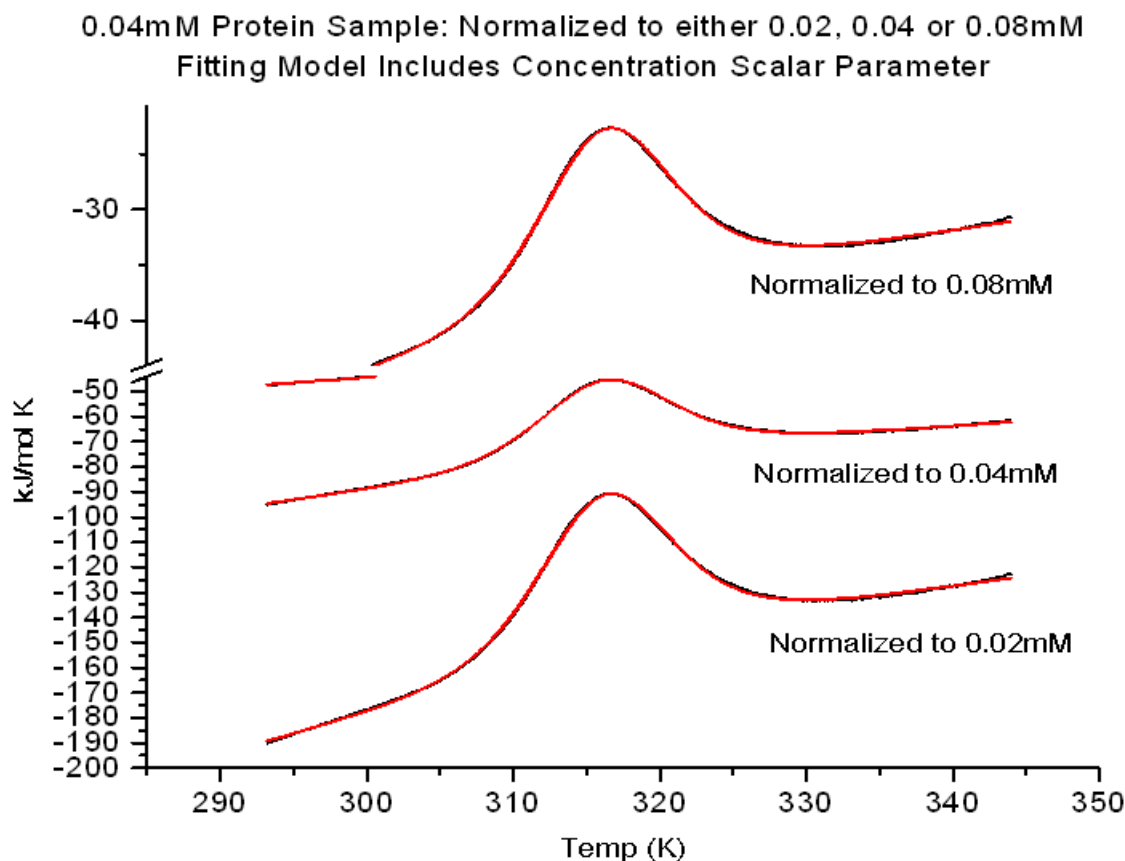
The fit overshoots the data normalized to 0.02mM (suggestive of a folding intermediate), fits reasonably well with the data normalized to 0.04mM (the "correct" concentration) and undershoots the data normalized to 0.08mM (suggestive of a van't Hoff enthalpy greater than the calorimetric, indicative of multimers in the native state). The refined parameters for the above fits are as follows:

Parameter	Normalized to 0.08mM	Normalized to 0.04mM	Normalized to 0.02mM
A ₀	0	0	0
A ₁	0	0	0
B ₀	106.399543	491.9808408	1310.731465
B ₁	142.2004446	146.4605106	12.70224628
C ₀	-42033.46479	-72659.20659	-133991.364
DCTD	3276.45386	1771.328293	3131.276108
DDTD	235633.051	297758.6783	385858.7965
TD	315.5935796	316.2024851	316.1545567

If a scalar is introduced into the basic expression for the heat capacity function the error in the normalization of the concentration can be corrected:

$$C(T) = \left(C_N(T) + \Delta C_p * (1 - F_N) + \left(\frac{H_{\varphi_s}(T)^2 * F_N * (1 - F_N)}{RT^2} \right) \right) / k$$

Here we are dividing our model for the experimentally observed heat capacity by the scalar term k . If the above three data sets are re-analyzed with this new model we get the following results:

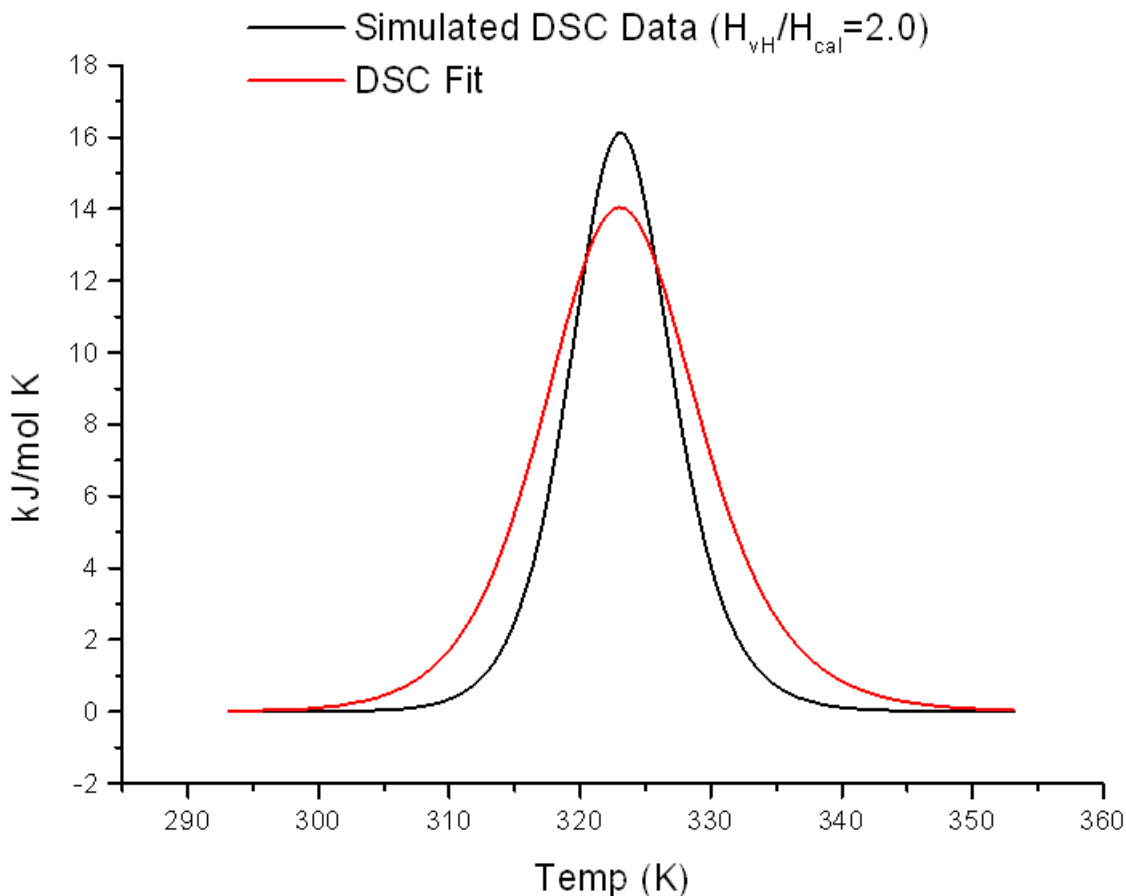


Parameter	Normalized to 0.08mM	Normalized to 0.04mM	Normalized to 0.02mM
A_0	0	0	0
A_1	0	0	0
B_0	305.4946027	305.4946039	305.4945983
B_1	152.5561894	152.5561889	152.5561915
C_0	-58243.45094	-58243.45113	-58243.45016
k	1.526433462	0.7632167336	0.3816083605
DCTD	2273.729531	2273.729583	2273.729321
DDTD	271551.4875	271551.4878	271551.4863
TD	316.0675458	316.0675458	316.0675458

The parameters refine to identical values except for the k parameter, which reflects the concentration error in the normalization. Why is the value for k not equal to 1.0 for the data set normalized to 0.04mM? One possibility is that our sample is not actually at 0.04mM (but is actually 0.052mM). Alternatively, the protein may not exhibit two-state denaturation, and thus, the *van't Hoff* and calorimetric enthalpies may not be equal (i.e. $\Delta H_{vH}/\Delta H_{cal}$ does not equal 1.0). How does a non-equality of the *van't Hoff* and calorimetric enthalpies affect the analysis?

Here is a fit to a simulated DSC run with the following parameters:

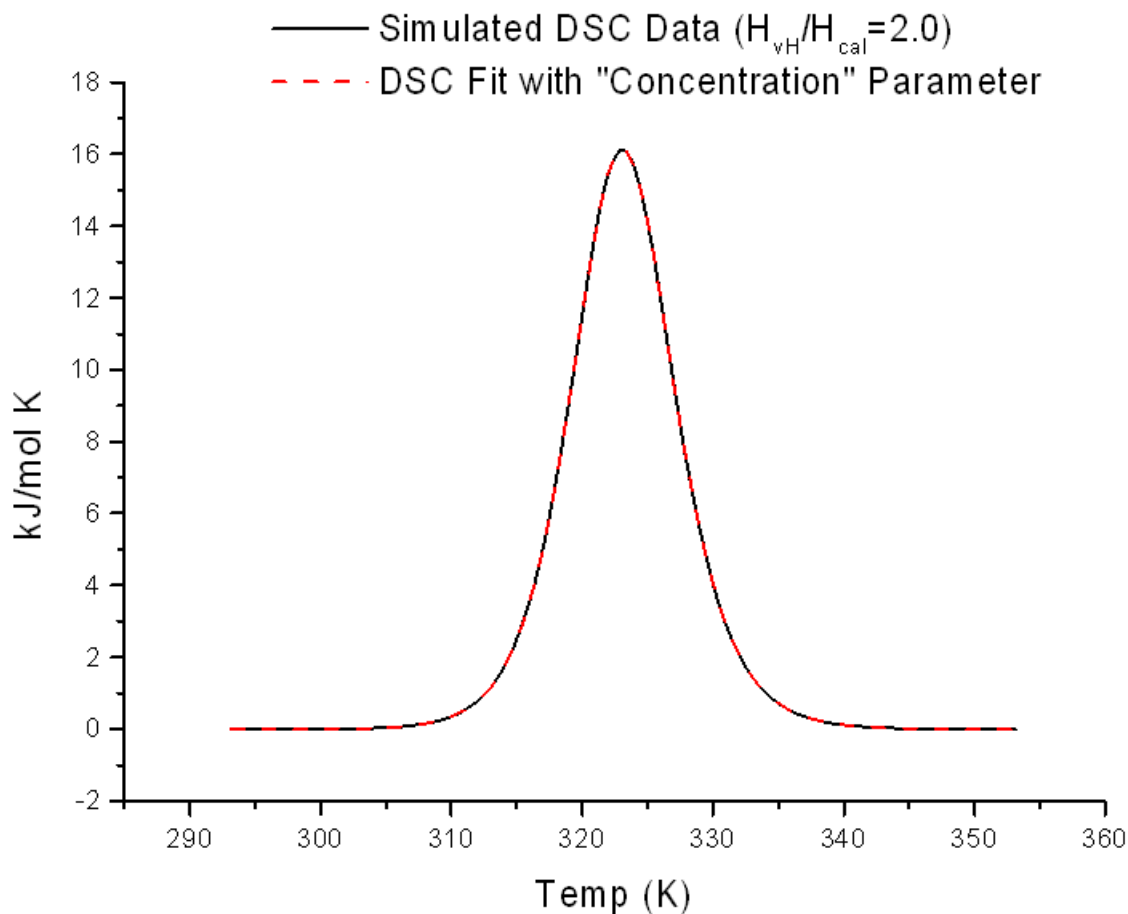
TD = 323.15 K, $H_{cal} = 167.4$ kJ/mol, $H_{vH} = 334.9$ kJ/mol, ($\Delta H_{vH}/\Delta H_{cal} = 2.0$), ($\Delta C_p = 0$, slopes for baselines = 0)



The fit undershoots the peak, indicating a situation where the $\Delta H_{vH}/\Delta H_{cal}$ is greater than 1.0 (with possible multimers in the native state). In any case, a two-state model does not fit the data. The parameters of the fit are:

Parameter	
A_0	0
A_1	0
B_0	0
B_1	0
C_0	0
DCTD	0
DDTD	220899.7025
TD	323.223306

What happens to the fit if we include the same scalar, k , as before? Here are the results of the fit:



Parameter	
A ₀	0
A ₁	0
B ₀	0
B ₁	0
C ₀	0
k	1.99901503
DCTD	0
DDTD	334715.0703
TD	323.1500011

In this case, DDTD agrees with the expected value for the **van't Hoff** enthalpy (334.9 kJ/mol). The value for the parameter *k* agrees with the ratio of $\Delta H_{vH}/\Delta H_{cal}$ (2.0). ΔH_{cal} can now be derived by dividing DDTD (*van't Hoff* enthalpy) by *k* ($\Delta H_{vH}/\Delta H_{cal}$), yielding 167.4 kJ/mol.

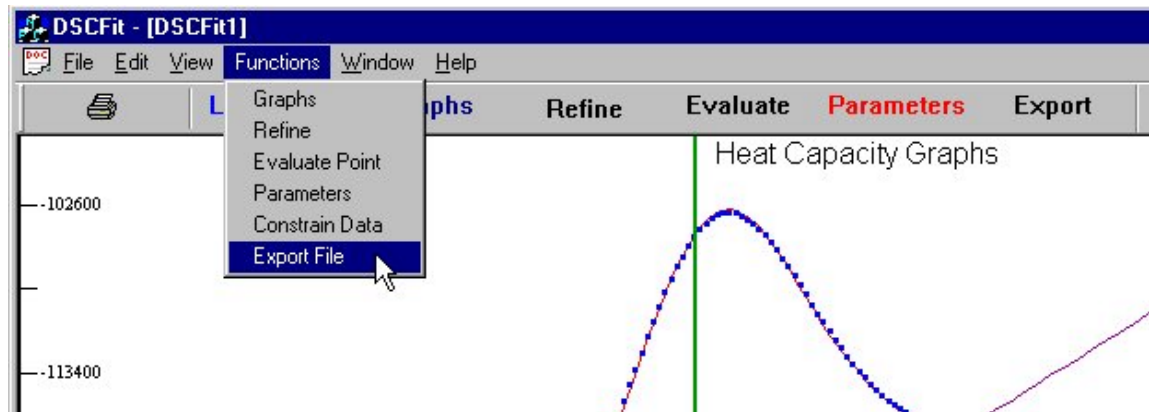
Conclusions:

- Errors in concentration or situations where the *van't Hoff* enthalpy do not agree with the calorimetric enthalpy can result in a similar situation - errors in enthalpy and deviation of the fit with a 2-state model
- Introduction of a scalar (*k*) in the model can correctly adjust the model for two situations: 1) errors in concentration (assuming *van't Hoff* and calorimetric

enthalpies are equal), and 2) determination of the van't Hoff to calorimetric enthalpy ratio (assuming concentration is correct).

Section 6: Output of Function Data for Use in Other Programs

Data associated with relevant thermodynamic functions can be output for use in other programs. This is particularly useful for presentation quality graphics. To output function data, choose the **Functions**→**Export File** command:



You will be given the option of adding comments to the top of the output file. You can output the file as either a text or .csv file (which can be read directly into popular spreadsheet programs). The output of a typical .csv file will look like this:

Ao	Bo	Co	A1	B1	DCTD	DDTD	TD	k		
0	99.9690	-121530	0	435.449	-6497.17	-257266	312.5667	1		
Temperature	Raw Data	C(T)	Residual Scatter	CpN(T)	CpD(T)	DCp(T)	DH(T)	DS(T)	DG(T)	F _N (T)
287.276	-149246	-148519.8	-726.19735	-126587	-150053	-23466	121631	451.06386	-7947.93	0.034633
287.55	-148989	-148426.5	-562.50016	-126532	-149814	-23282	115227	428.78033	-8068.47	0.033087
287.823	-148713	-148316.5	-396.49734	-126477	-149577	-23099	108896	406.77338	-8182.52	0.031694
288.097	-148446	-148191.07	-254.92639	-126422	-149338	-22915	102592	384.8814	-8290.97	0.03043
288.373	-148220	-148051.33	-168.67178	-126367	-149098	-22730	96293	363.02736	-8394.17	0.029279

This output data includes the input raw data, fitted Cp(T) function, residual scatter, native and denatured state baselines, $\Delta C_p(T)$, $\Delta H(T)$, $\Delta S(T)$, $\Delta G(T)$ and F_N(T) (fraction native state) functions.

References

Kidokoro, S.-I. and A. Wada (1987). "Determination of thermodynamic functions from scanning calorimetry data." Biopolymers **26**: 213-229

Freire, E. and Biltonen, R.L. (1978). "Statistical mechanical deconvolution of thermal transitions in macromolecules. I. Theory and application to homogeneous systems." Biopolymers **17**:463-479

Referencing DSCFit in your publications

Details of the DSCFit program have been published in the following:

An Efficient, Flexible-Model Program for the Analysis of Differential Scanning Calorimetry Data, Grek, S., Davis, J. and Blaber, M. *Protein and Peptide Letters* **6**, 429-436 (2001)